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# Investigation of Hydrogen Evolution at Negative Electrode for a Vanadium Redox Flow Battery

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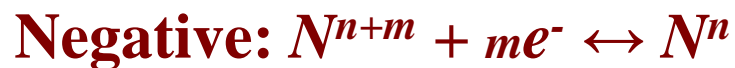
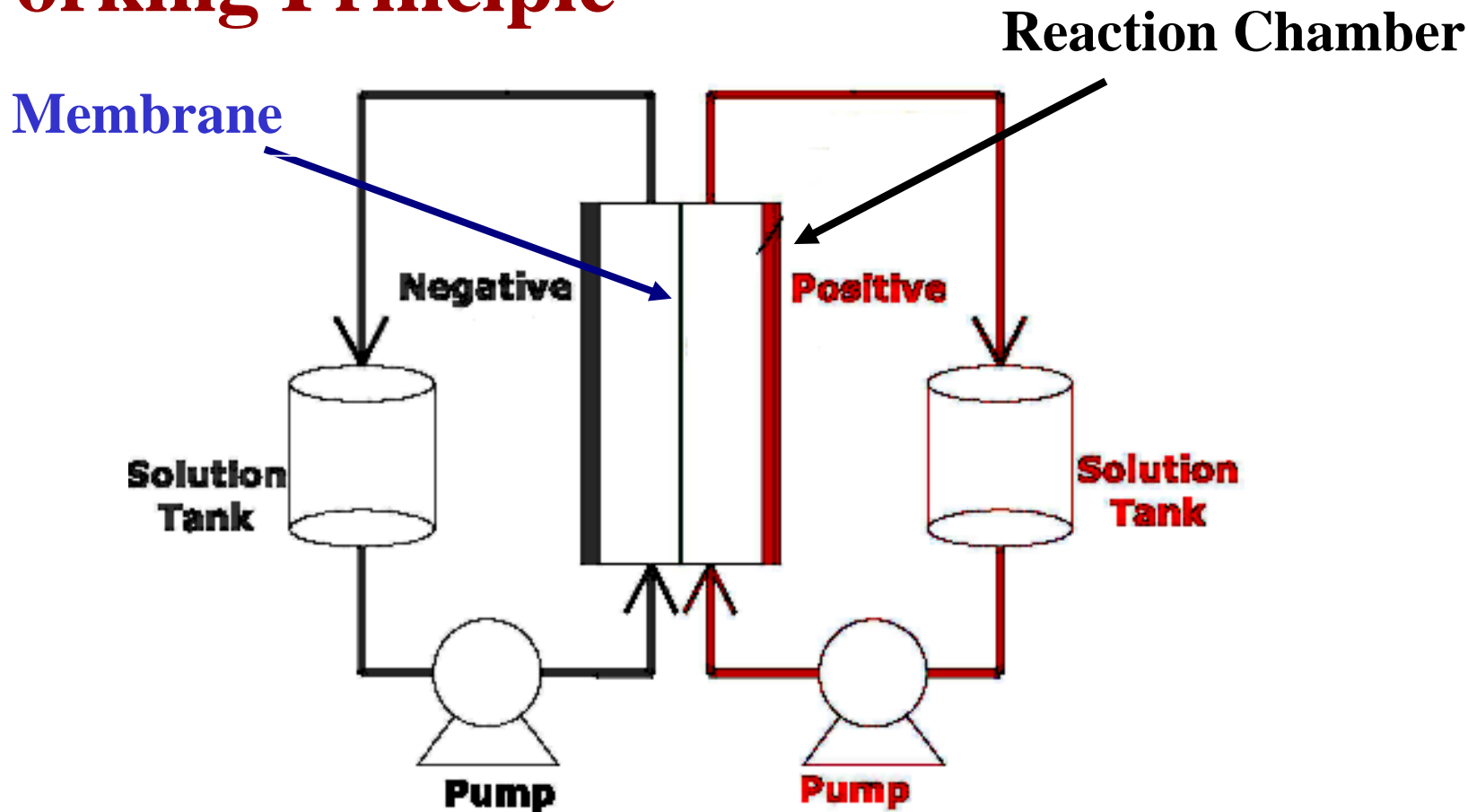
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# Outline

- **Introduction**
- **Experimental**
  - **Charging and Discharging Battery**
    - **Two Features**
  - **Hydrogen Evolution during Preparation of Anolyte**
    - **Intermediate Specie and Possible Mechanism**
  - **Spectrometry Study (Recent Study)**
    - **Spectrum and Applications**
- **Future Study**

# Working Principle



**Electrical Energy  $\Leftrightarrow$  Chemical Energy  $\Leftrightarrow$  Storage**

# Vanadium Redox Flow System (VRFS)

- VRFS has been studied for 25 years
- Positive  $V^{IV}/V^{V}$ :  $VO^{2+} + 2H^+ + e^- = VO^{++} + H_2O$
- Negative  $V^{II}/V^{III}$ :  $V^{++} = V^{+++} + e^-$
- 3 M  $H_2SO_4$
- Separated by proton-conducting membrane (*Nafion*)
- Carbon or Graphite Felt

## Advantageous:

- Cross-contamination problems **minimized**

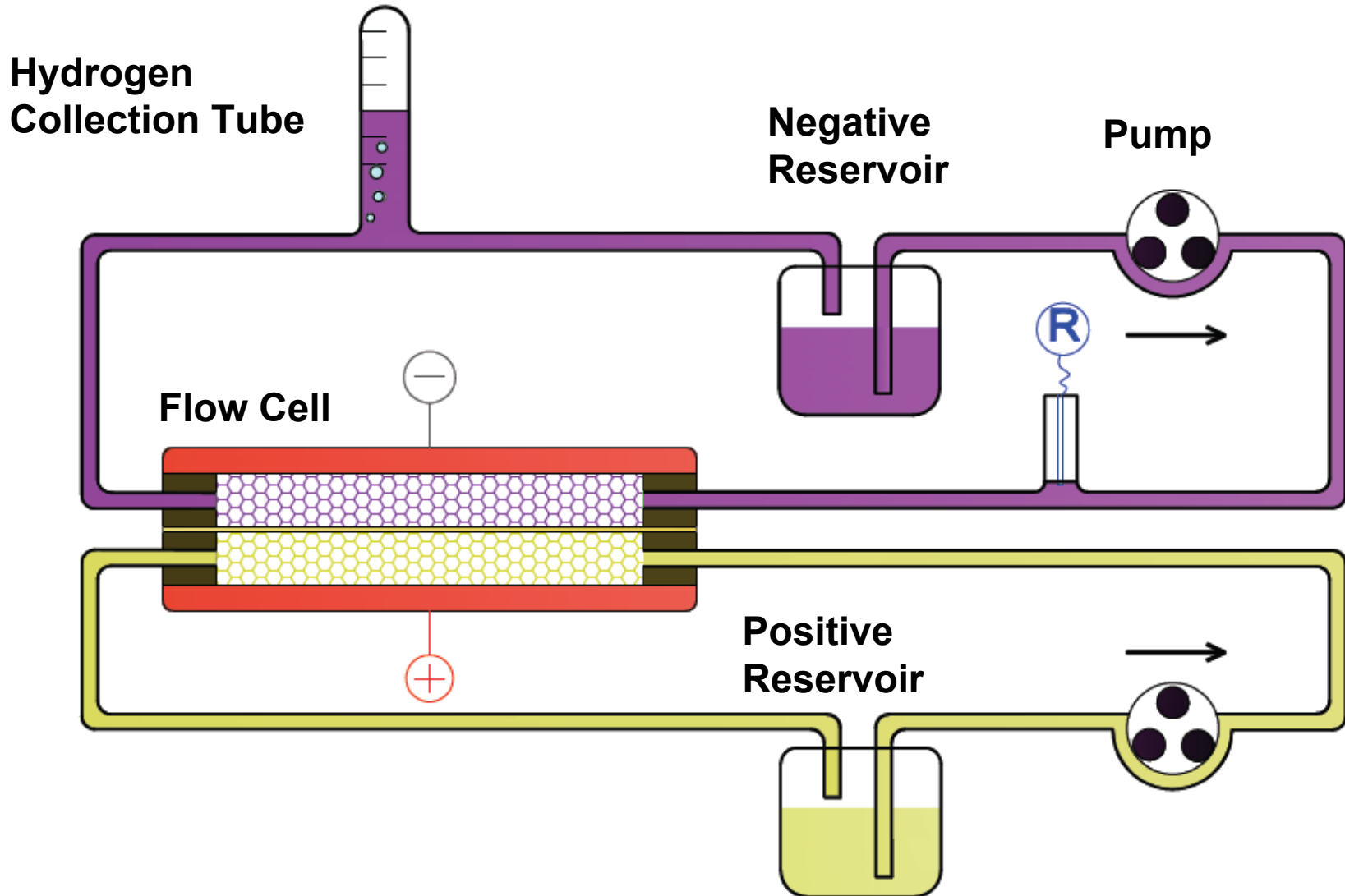
# Applications

More than 20 VRF battery systems have already been completed in Asia, Europe and the U.S.A..

1. 200 kW/ 800 kWh installed by Mitsubishi Chemicals (1996) at Kashima-Kita Electric Power, Japan for **load-levelling**.
2. 450 kW/ 900 kWh installed by Sumitomo Electric Industry (SEI) (1996) at Tasumi Sub-Station, Kansai Electric, Japan for **peak shaving**.
3. 250 kW/500 kWh installed by VRB Power (2001) at Stellenbosch University for ESKOM Power Corporation, South Africa for peak shaving and **UPS back-up power**.

<http://www.ceic.unsw.edu.au/centers/vrb/plist.htm>

# Experimental Setup



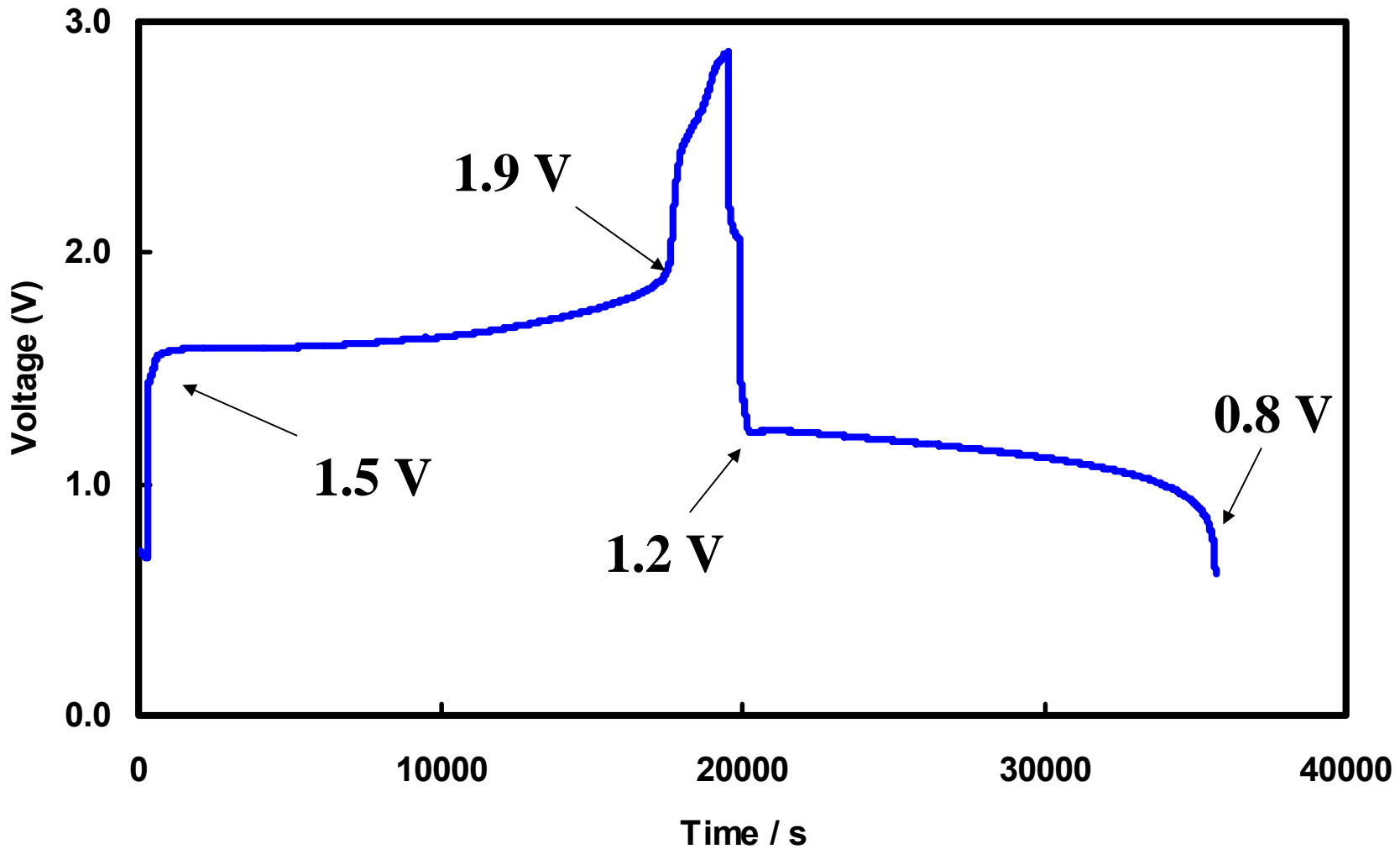
# Experimental Conditions

- **Flow Cell**
  - Big Cell: 16.24 cm<sup>2</sup>
  - Small Cell: 5.25 cm<sup>2</sup>
- **Flow Rate**
  - 0.44 cm<sup>3</sup> s<sup>-1</sup>
  - 0.15 cm<sup>3</sup> s<sup>-1</sup>
- **Temperature**
  - Reservoir: 25 °C
  - Room: 16 ~ 22 °C
- **Reference Electrode**
  - Hg/Hg<sub>2</sub>SO<sub>4</sub> (SME)

# Charging and Discharging Battery

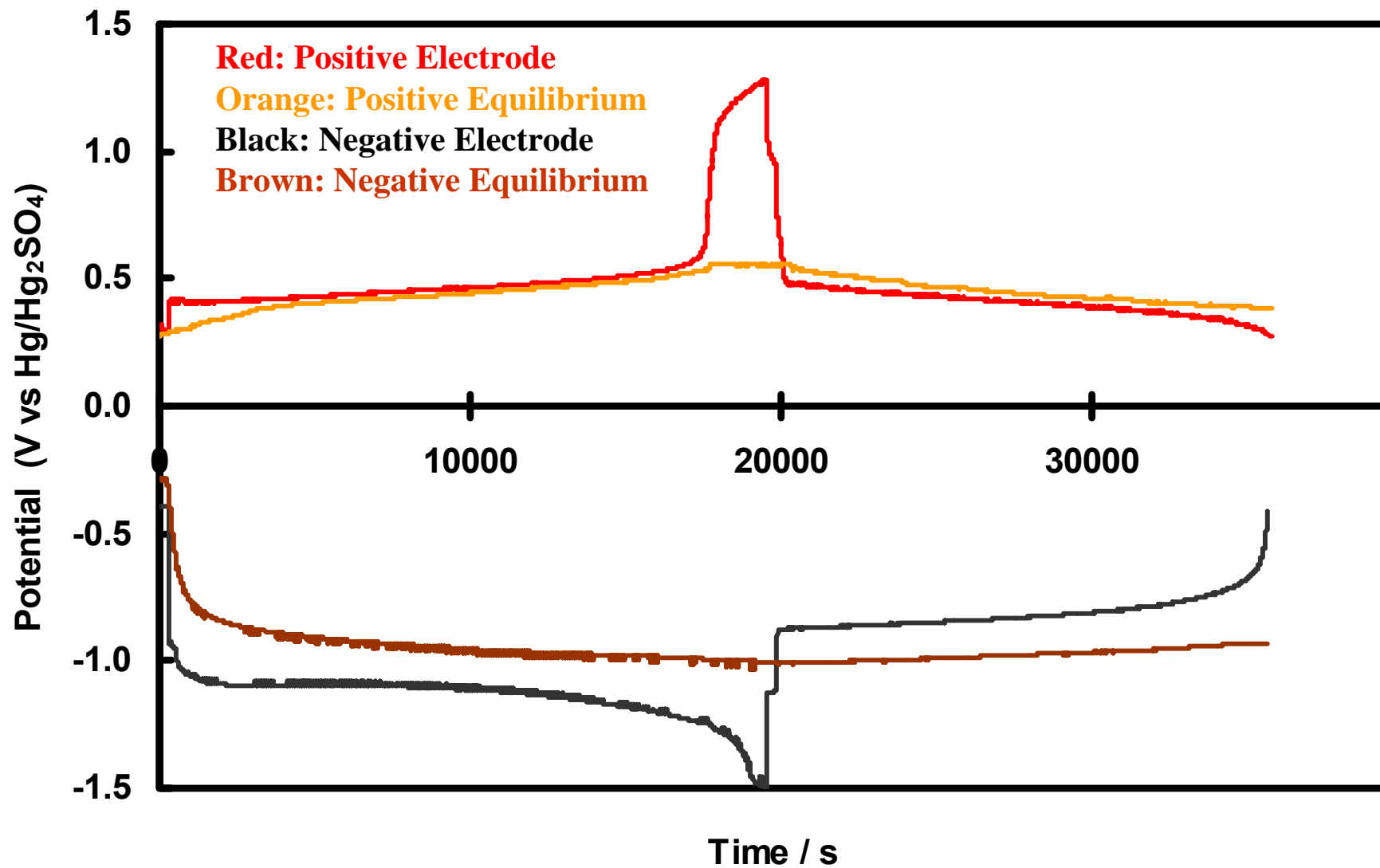


# Full Charging and Discharging Curve, Battery Voltage, 40 mA cm<sup>-2</sup>, 1.5 M Vanadium Solution in 3 M H<sub>2</sub>SO<sub>4</sub>

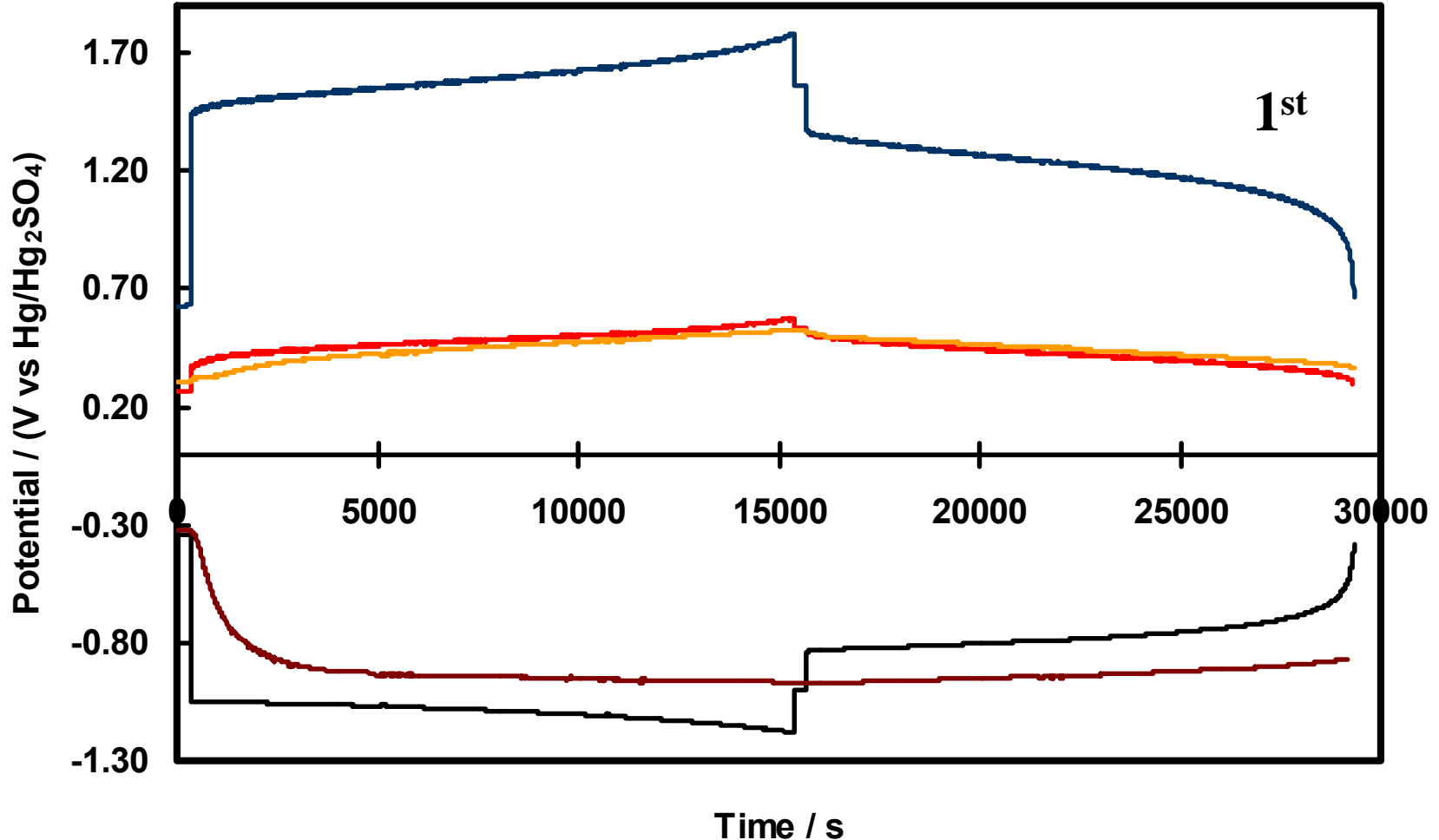


Coulombic efficiency is around 90% whereas voltage efficiency is only **55%**.

# Full Charging and Discharging Curve, 40 mA cm<sup>-2</sup>, Positive and Negative Electrodes, 1.5 M Vanadium Solution in 3 M H<sub>2</sub>SO<sub>4</sub>

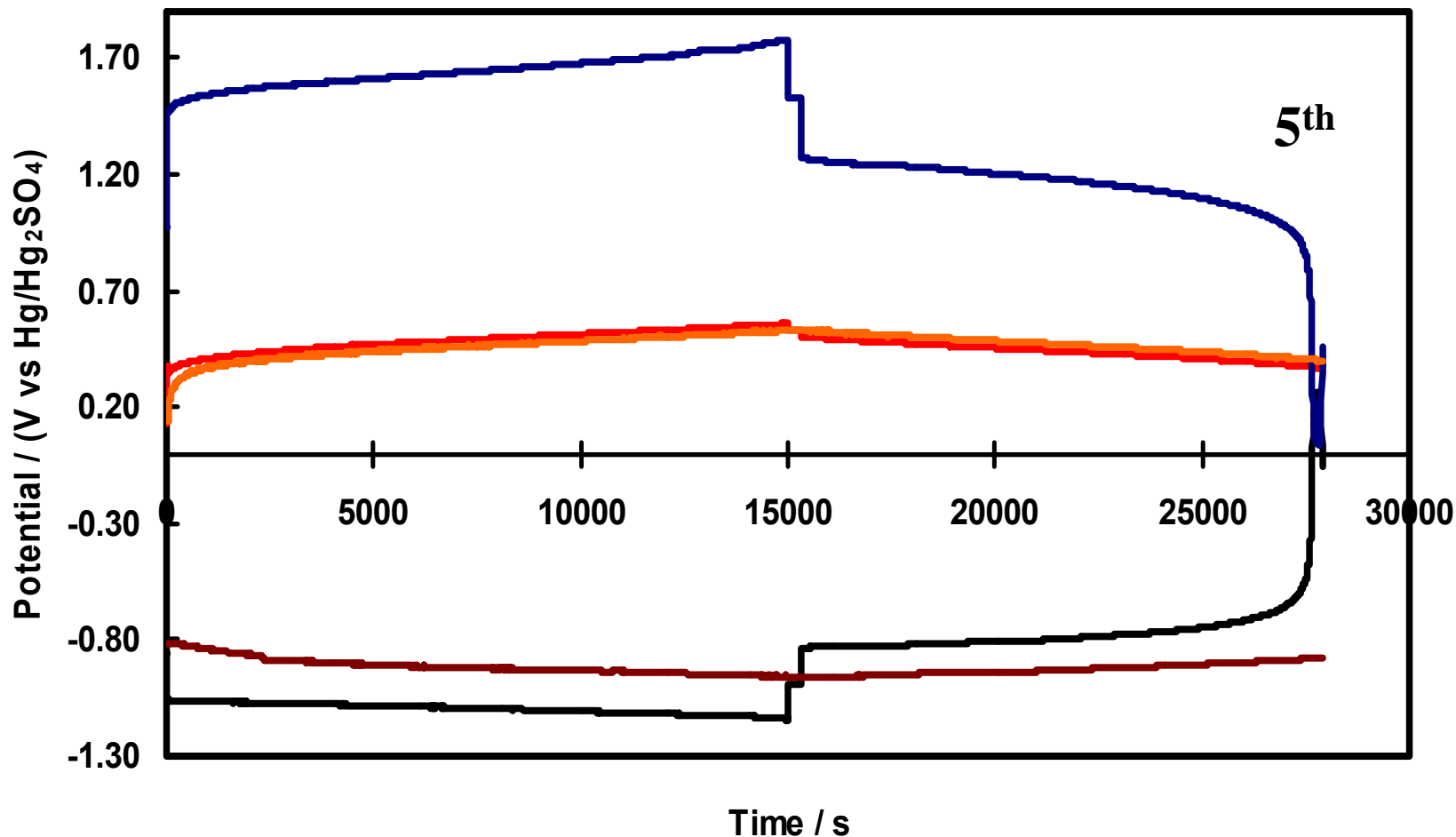


# Charging and Discharging Curves, $40 \text{ mA cm}^{-2}$ , $1.5 \text{ M Vanadium Solution in } 3 \text{ M H}_2\text{SO}_4$



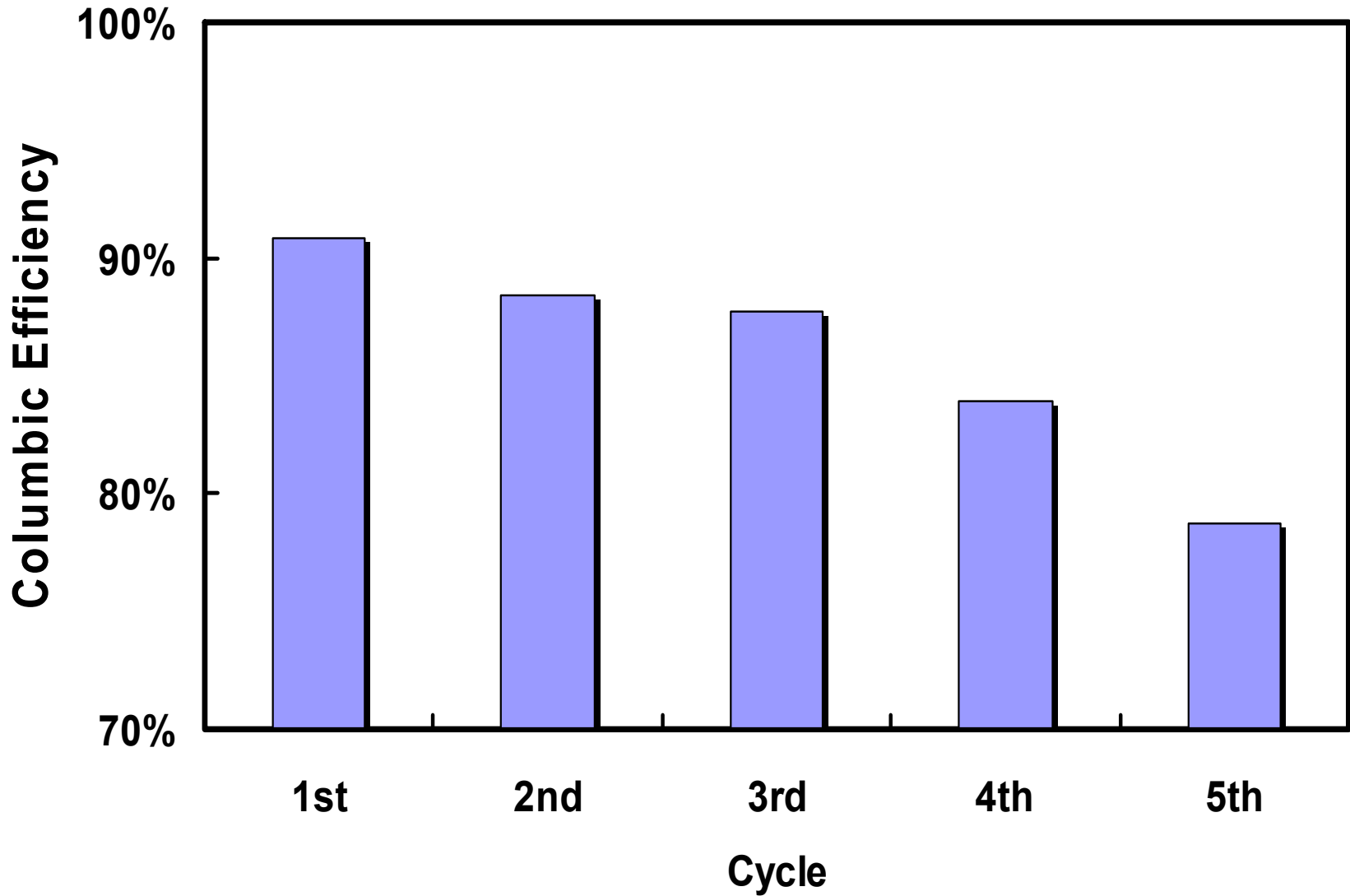
Coulombic efficiency is around 92%

# Charging and Discharging Curves, 40 mA cm<sup>-2</sup>, 1.5 M Vanadium Solution in 3 M H<sub>2</sub>SO<sub>4</sub>



Coulombic efficiency is around 78%

# Columbic Efficiency



# Conclusions

- Negative overpotential is bigger than positive overpotential.
- Battery's life is limited by the negative electrode.
- **Hydrogen is formed at the negative electrode.**

# **\* Hydrogen Evolution during Preparation of Anolyte**

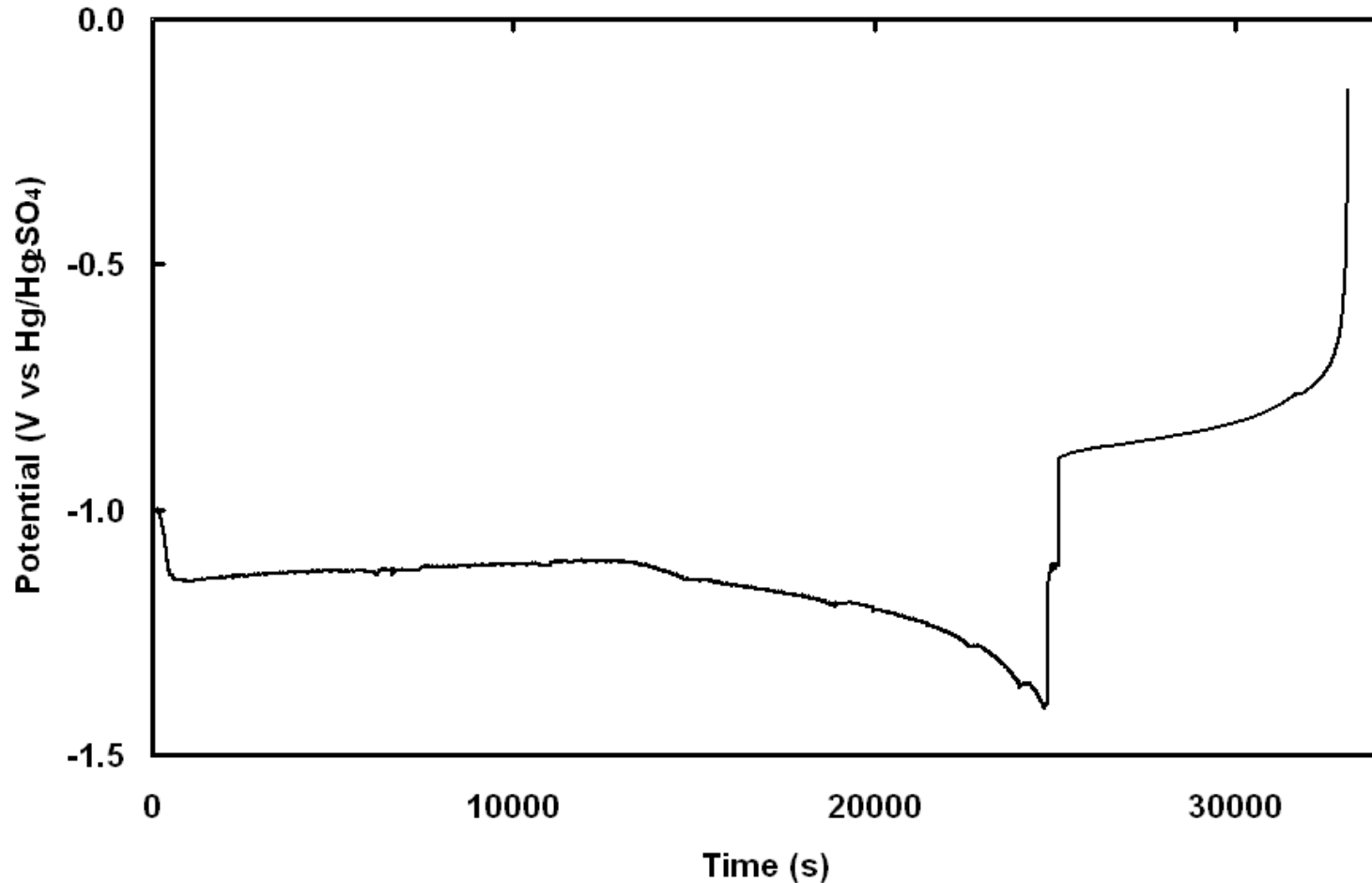
**\*This result has been first presented by Prof. D. N. Buckley on ECS Meeting 2010, Vancouver, BC, Canada.**

# Reduction of $\text{VO}^{++}$ and $\text{V}^{+++}$

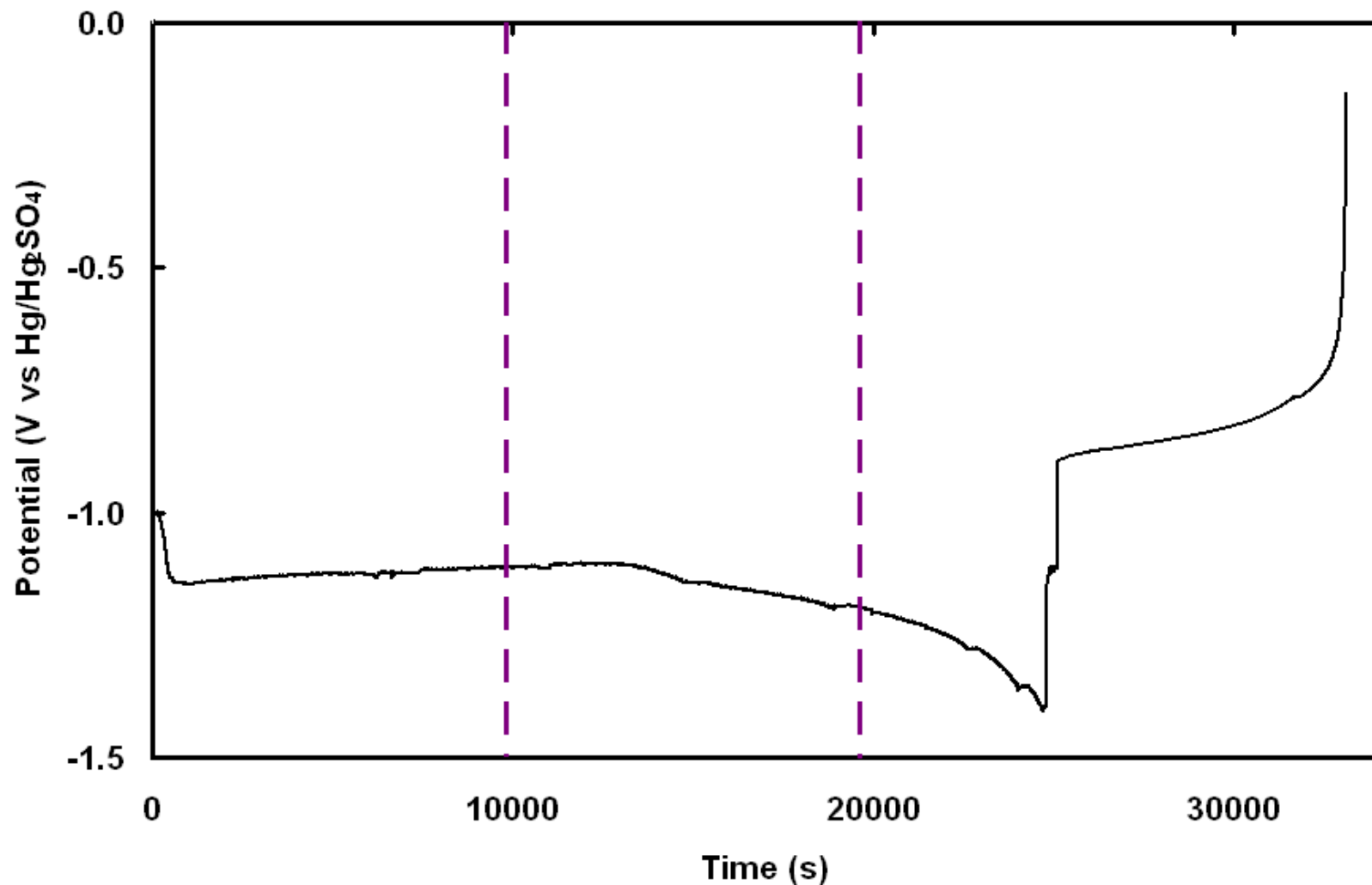
- $\text{VO}^{++} + 2\text{H}^+ + \text{e}^- = \text{V}^{+++} + \text{H}_2\text{O}$ 
  - $E_0 = 0.337 \text{ V (SHE)}$
  - $= -0.303 \text{ V (SME)}$
  - High overpotential
- $\text{V}^{+++} + \text{e}^- = \text{V}^{++}$ 
  - $E_0 = -0.291 \text{ V (SHE)}$
  - $= -0.931 \text{ V (SME)}$
- Thermodynamically expect hydrogen



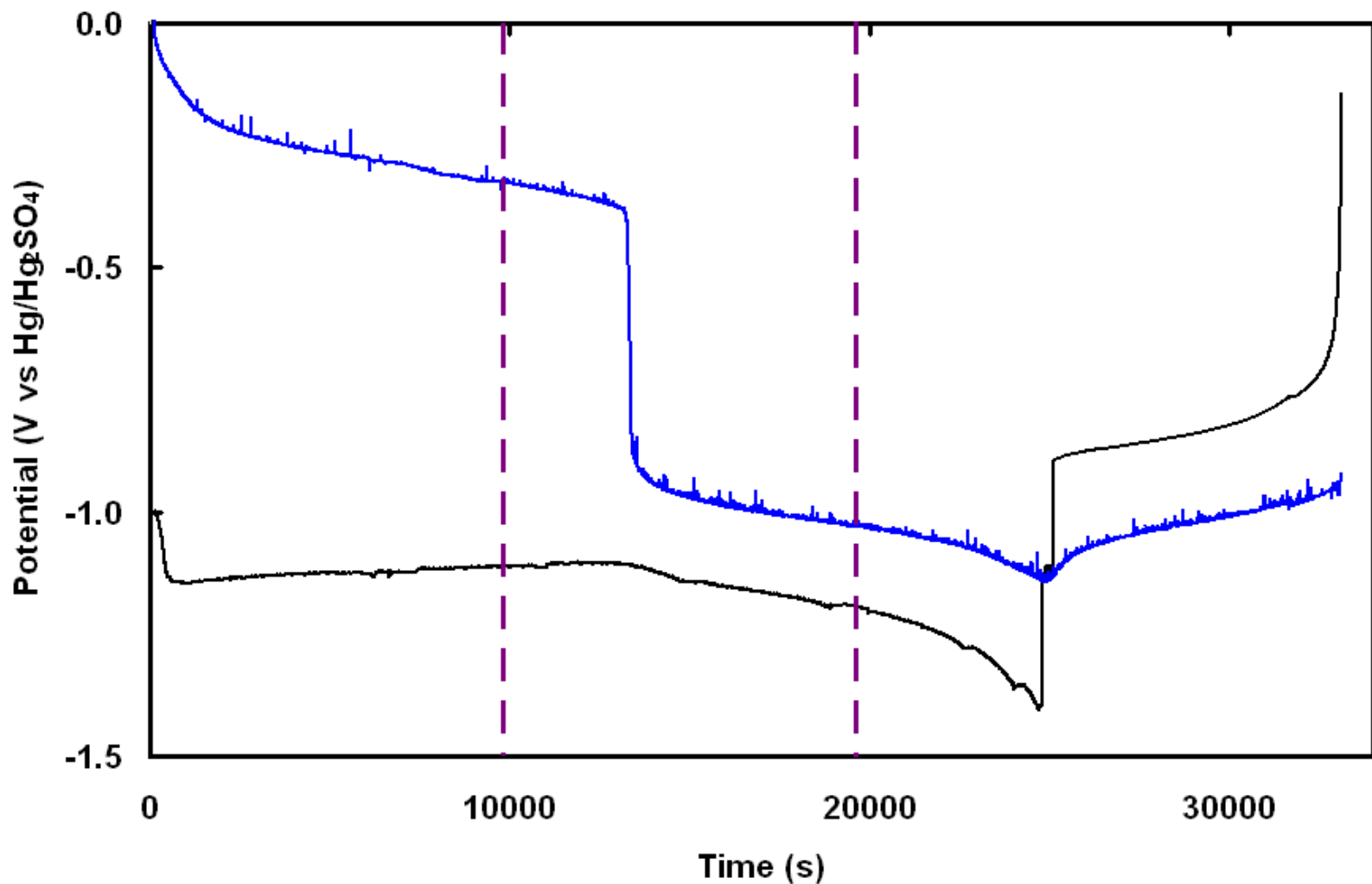
# Charging Curve, Negative Electrode, $40 \text{ mA cm}^{-2}$ , $1.5 \text{ M VO}_2\text{SO}_4$ in $3 \text{ M H}_2\text{SO}_4$



# Charging Curve, Negative Electrode, 40 mA cm<sup>-2</sup>, 1.5 M VOSO<sub>4</sub> in 3 M H<sub>2</sub>SO<sub>4</sub>



# Charging Curve, Negative Electrode, 40 mA cm<sup>-2</sup>, 1.5 M VOSO<sub>4</sub> in 3 M H<sub>2</sub>SO<sub>4</sub>



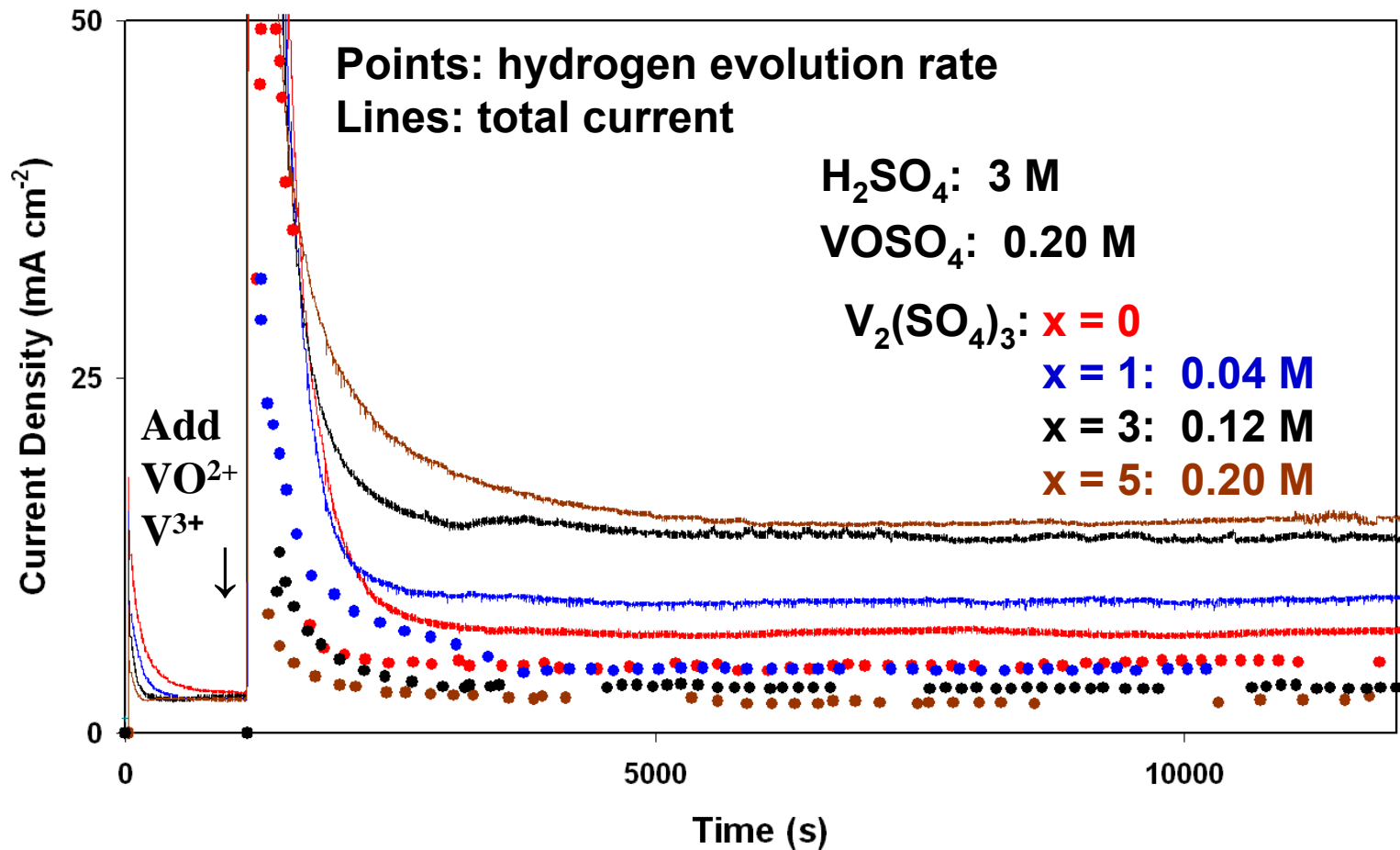
# Addition of $\text{VO}^{2+}/\text{V}^{3+}$ to 3 M $\text{H}_2\text{SO}_4$

Potential:  $-1.05$  V (Hg/ $\text{Hg}_2\text{SO}_4$ )

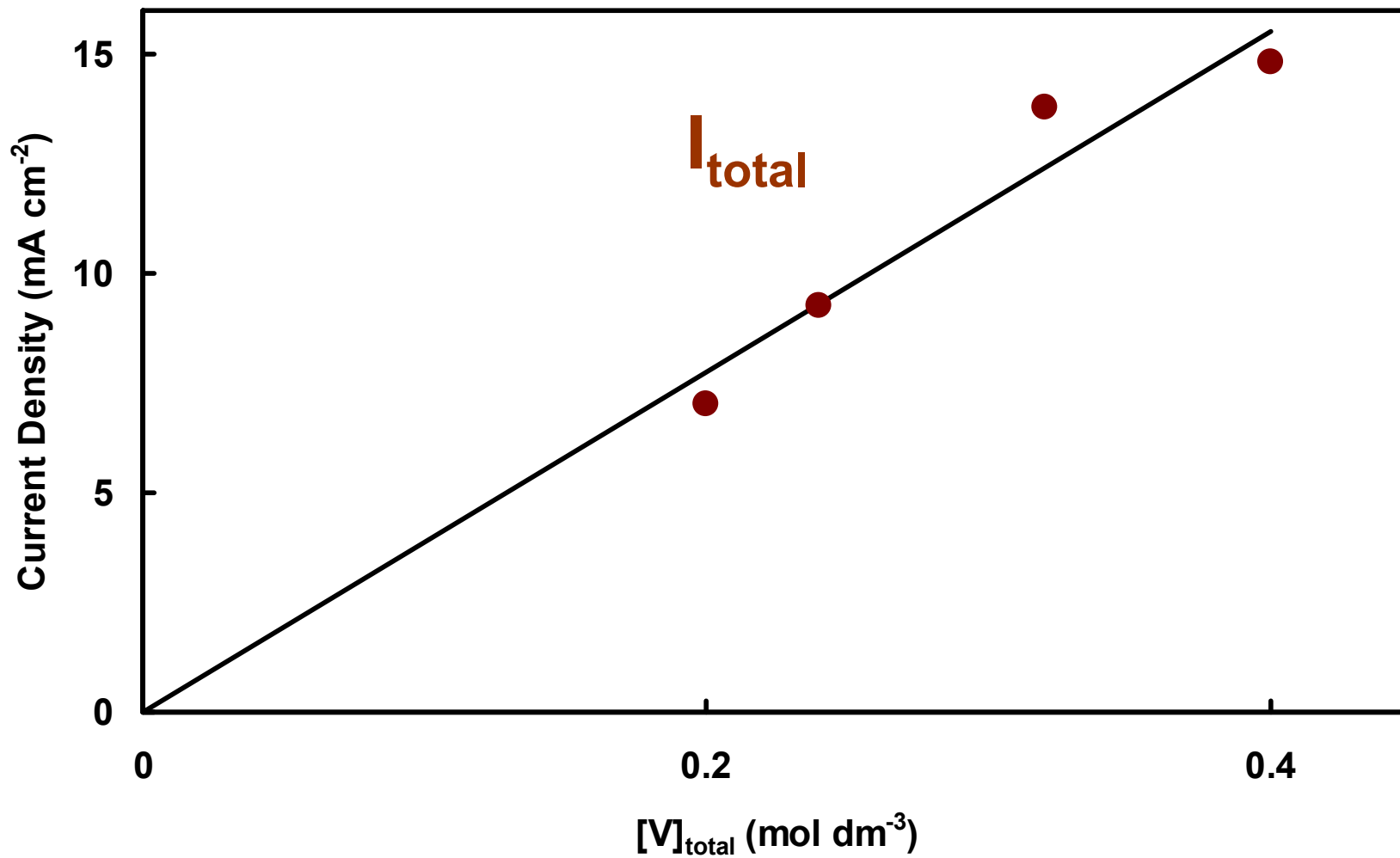
Add 12.5 mL to 25 mL 3 M  $\text{H}_2\text{SO}_4$

(5 mL 1.5 M  $\text{VOSO}_4$  + x mL 1.5 M  $\text{V}_2(\text{SO}_4)_3$ ;

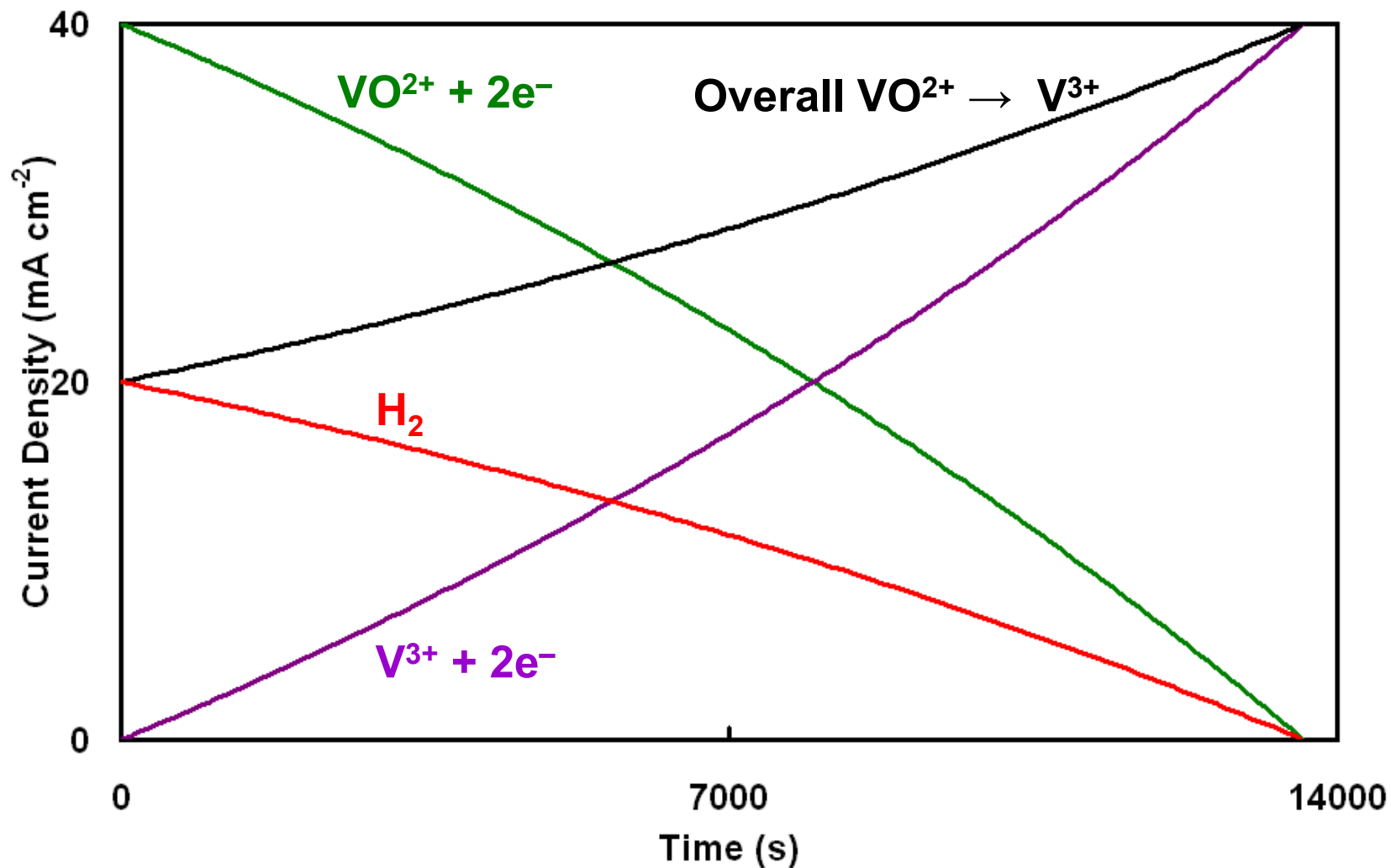
balance to 12.5 mL;  $[\text{H}_2\text{SO}_4] = 3$  M)



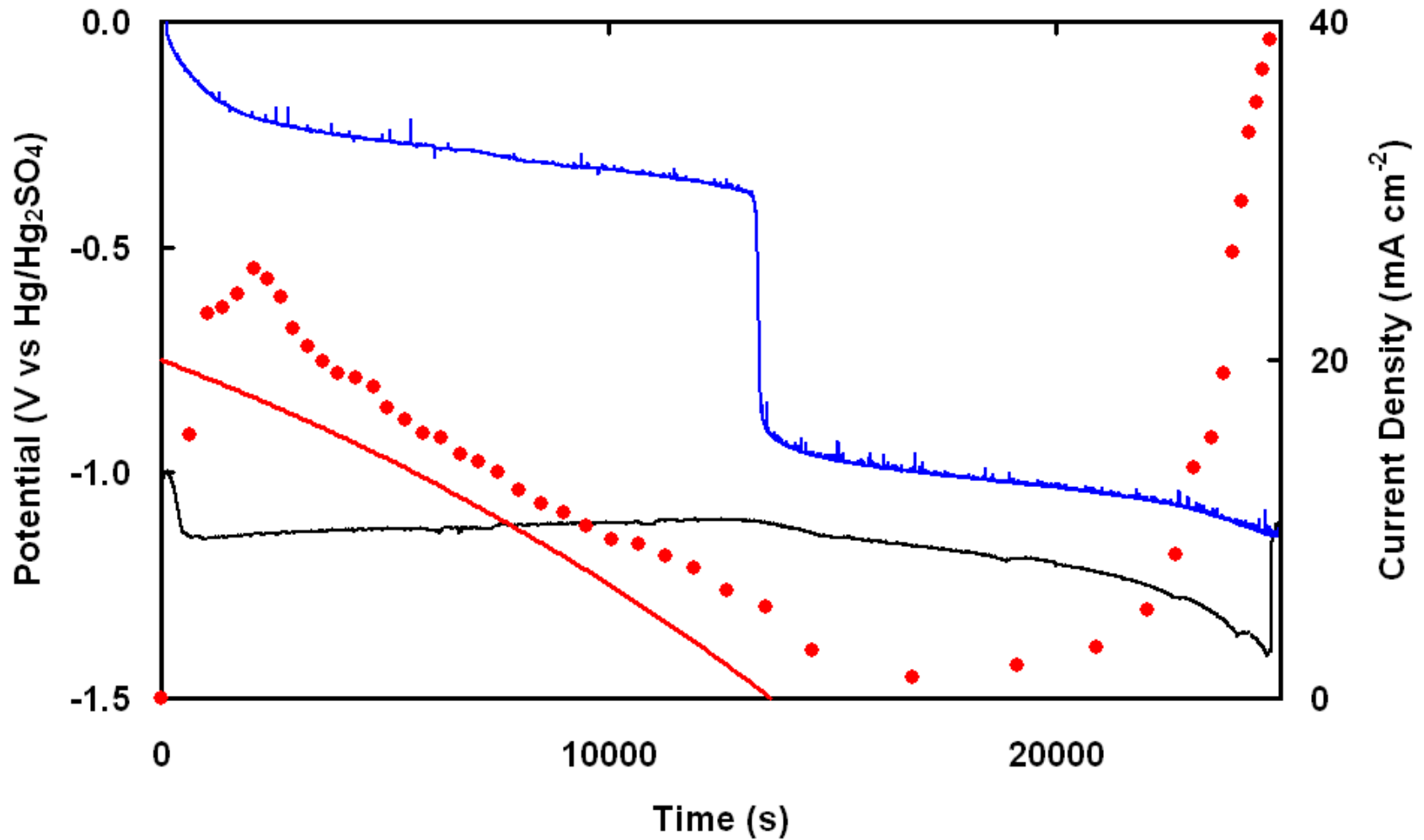
# Addition of $\text{VO}^{2+}/\text{V}^{3+}$ to 3 M $\text{H}_2\text{SO}_4$



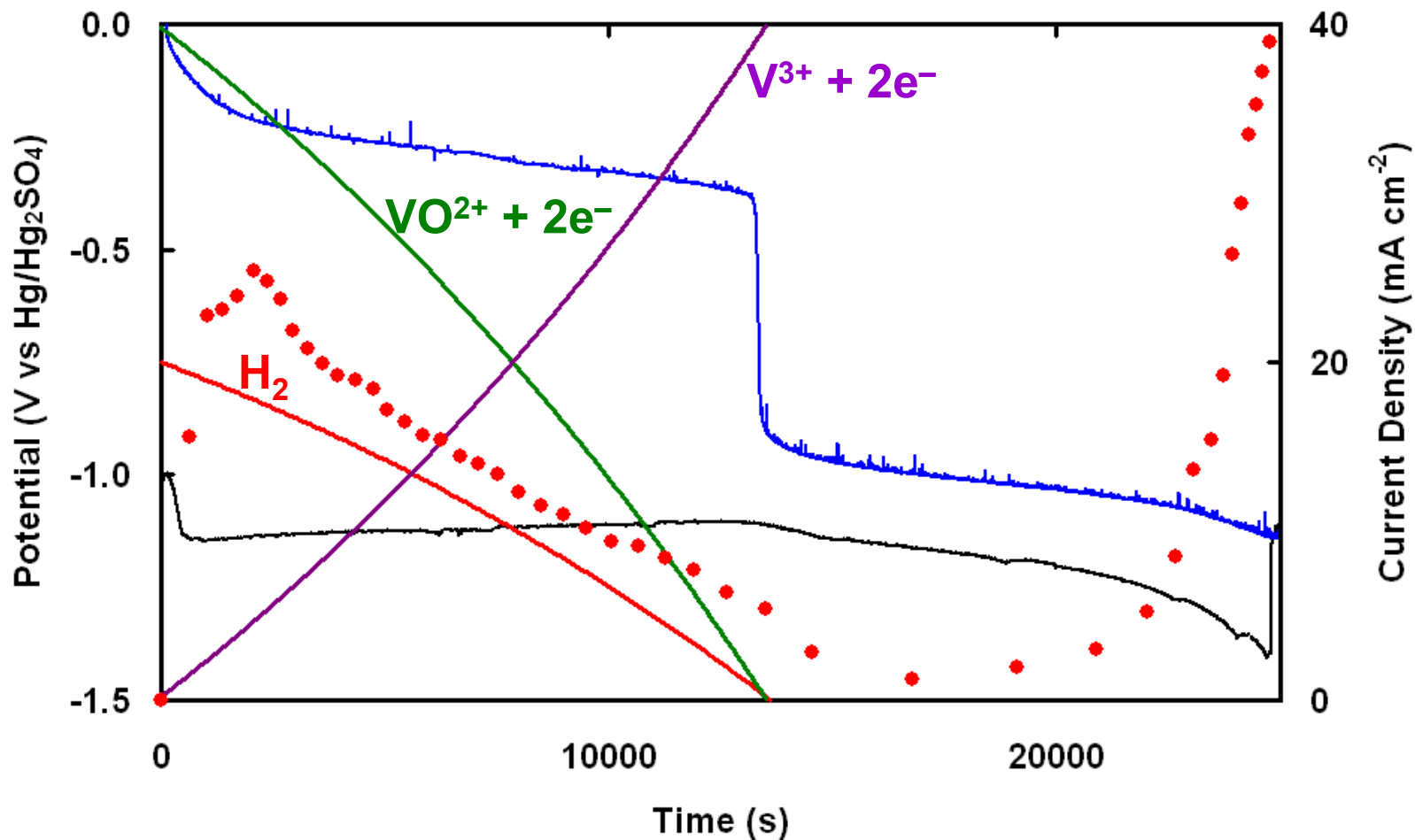
# Model Predictions: $\text{VO}^{2+}$ Reduction and Hydrogen Evolution



# Comparison with Experiment



# Comparison with Experiment





# Conclusions

- Presence of  $\text{VO}^{++}$  enhances hydrogen evolution on carbon felt in 3 M  $\text{H}_2\text{SO}_4$
- Formation of a reactive intermediate  $\text{V}^{\text{II}}$
- Simple model gives reasonable agreement with results

# **Spectrometry Study**

• **The colour of Vanadium ions in  $\text{H}_2\text{SO}_4$  show:**

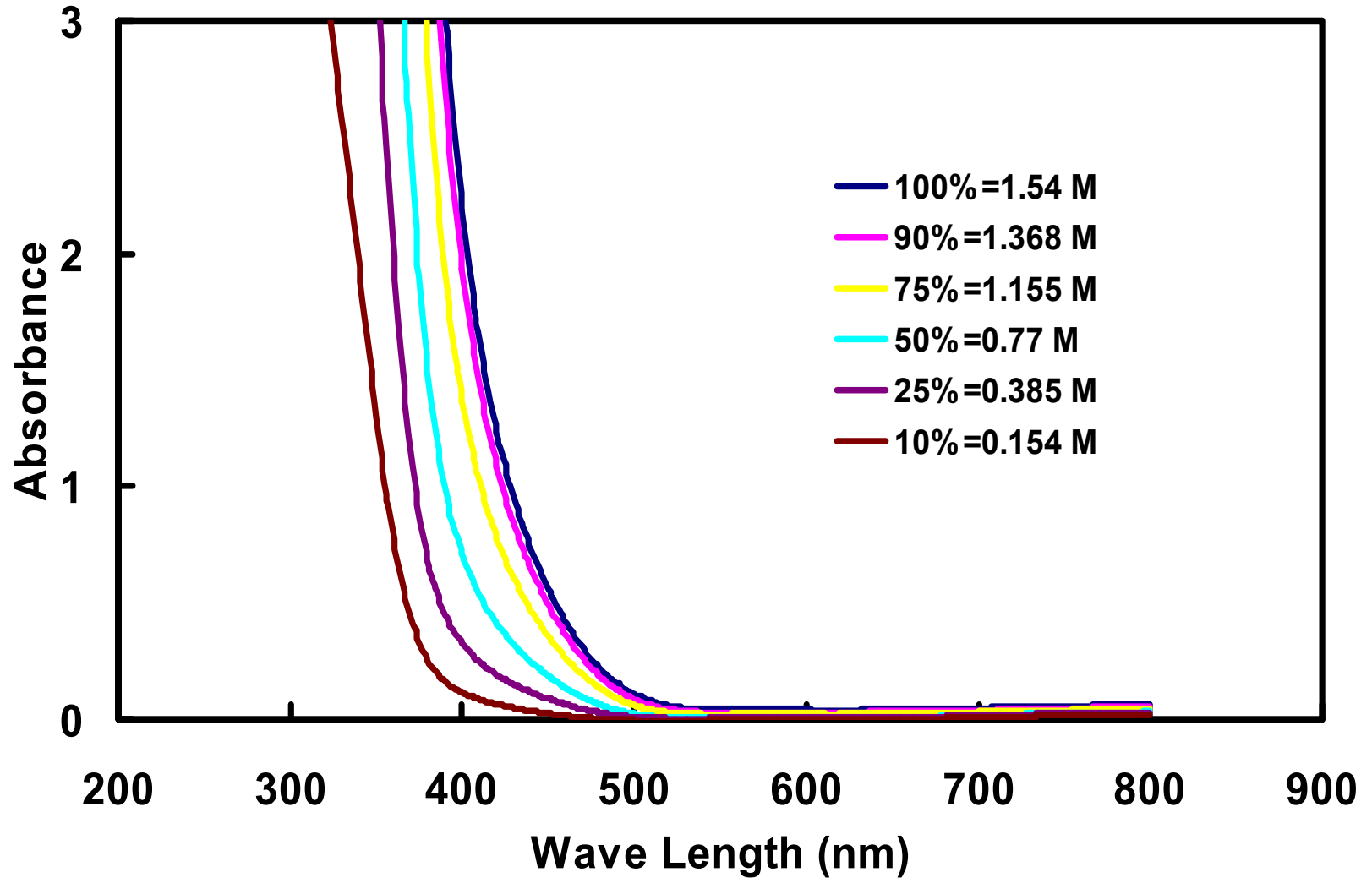
➤  **$\text{V}^{\text{V}}$ : Yellow**

➤  **$\text{V}^{\text{IV}}$ : Blue**

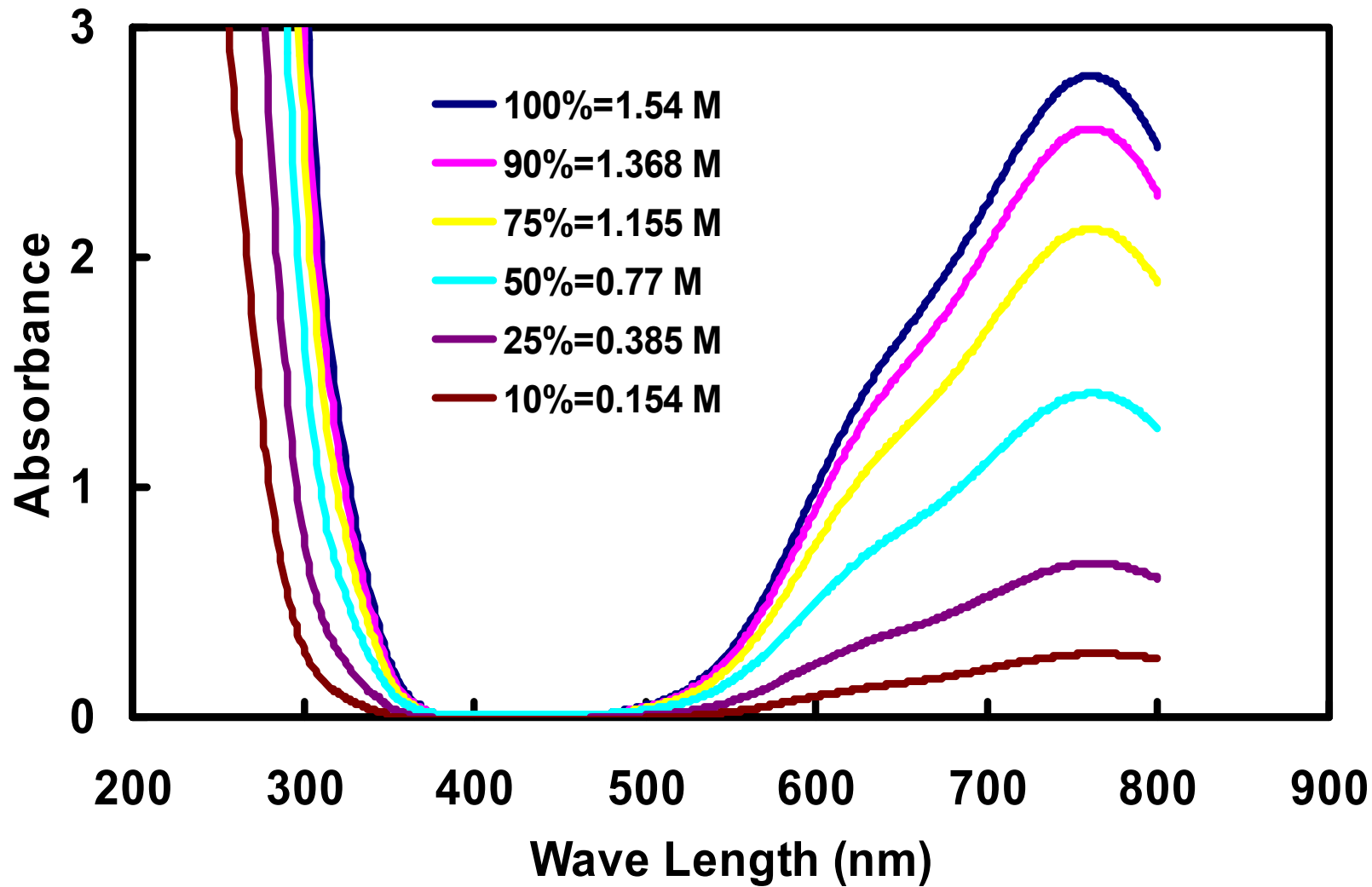
➤  **$\text{V}^{\text{III}}$ : Green**

➤  **$\text{V}^{\text{II}}$ : Purple**

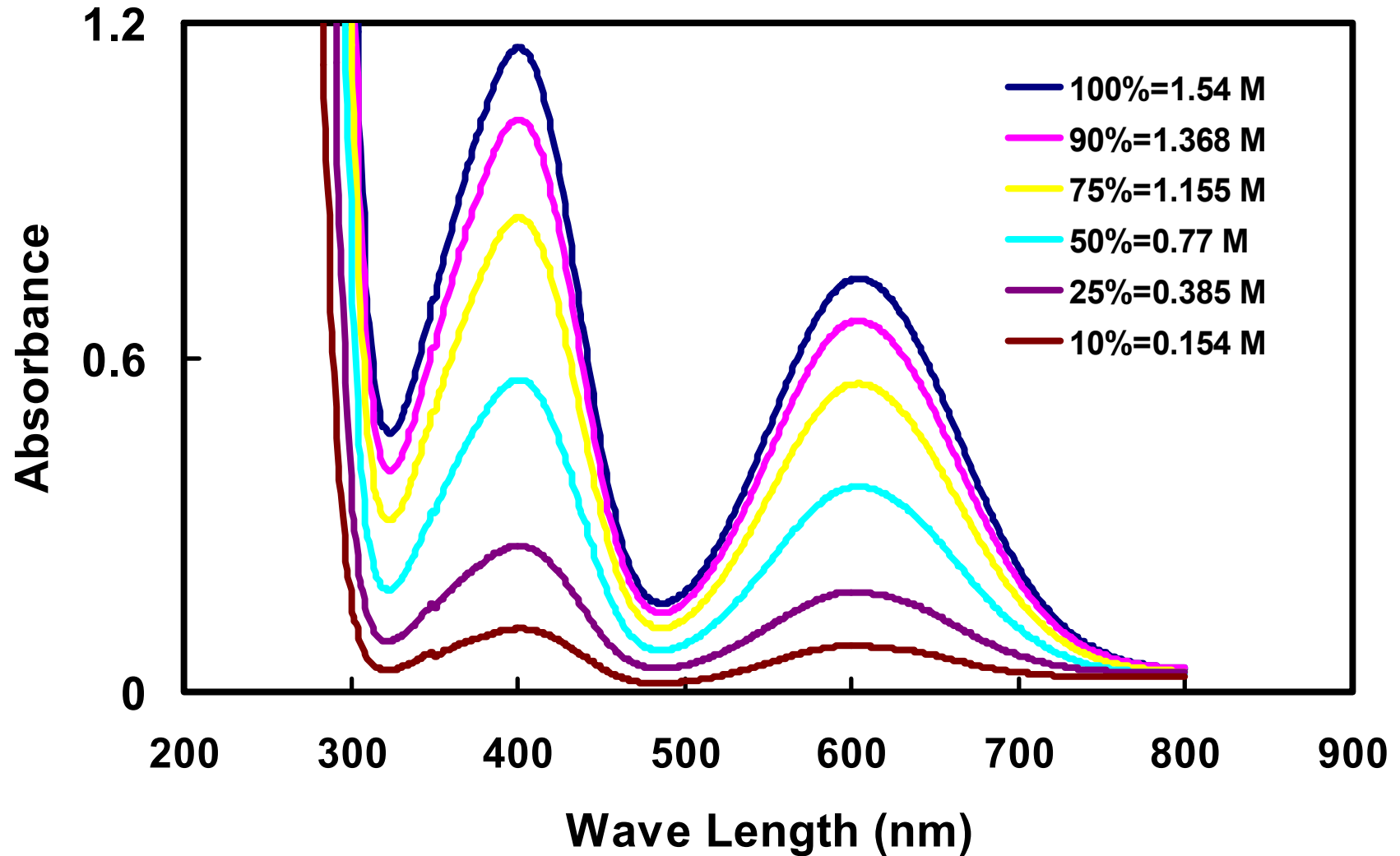
# V<sup>V</sup> Spectrum



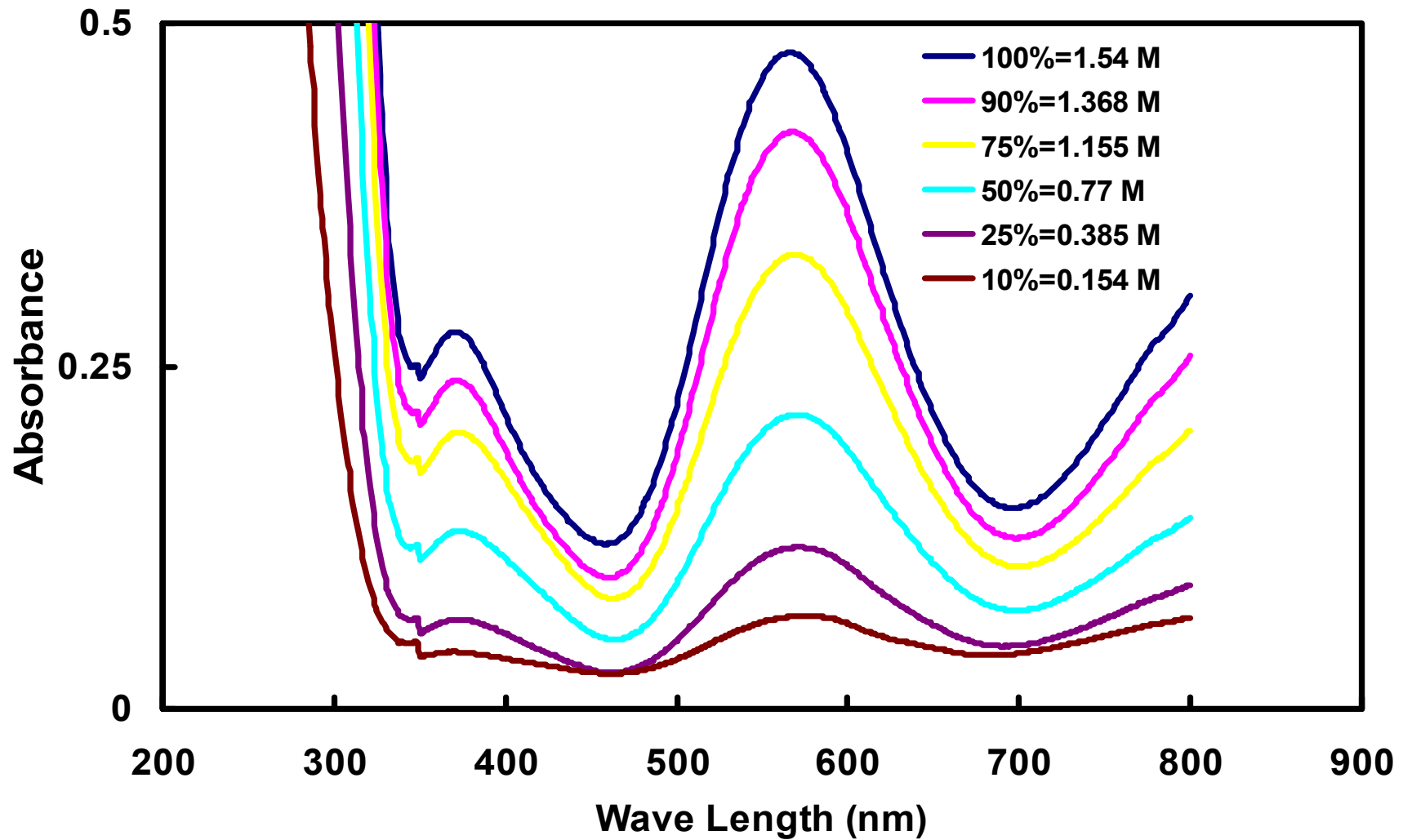
# V<sup>IV</sup> Spectrum



# V<sup>III</sup> Spectrum



# V<sup>II</sup> Spectrum



# **Future Work**

- **State of Charge**
- **Chemical titration**
- **Cyclic Voltammetry**
- **Chemical treatment of carbon felt**
- **Battery design**



# Acknowledgements



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